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SHANGHAI JIAO TONG UNIVERSITY



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# Bio-oil Production from Biomass Fast Pyrolysis and its Upgrading

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## There are 8 main parts

1. Introduction to Shanghai Jiao Tong University (SJTU)
2. Mechanism of biomass pyrolysis
3. Rotating cone reactor
4. Fluidized bed reactor for biomass fast pyrolysis for bio-oil production developed by SJTU
5. Performance of a commercial-scale biomass fast pyrolysis plant for bio-oil production
6. Hydrodeoxygenation (HDO) of Bio-oil
7. Other Biomass Energy Research in SJTU
8. Selected Publications (SCI)



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# 1.Introduction to Shanghai JiaoTong University(SJTU)

## ◆ Established in 1896

◆ There are 29 schools, including school of Agriculture and Biology, School of Mechanical and Power Engineering, etc.

◆ Students:49,838(Undergraduate16,221,graduate30,895, foreign student2,722);  
Teachers:3,014

◆Area of campus: about 333 ha.





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## School of Agriculture and Biology (SJTU)

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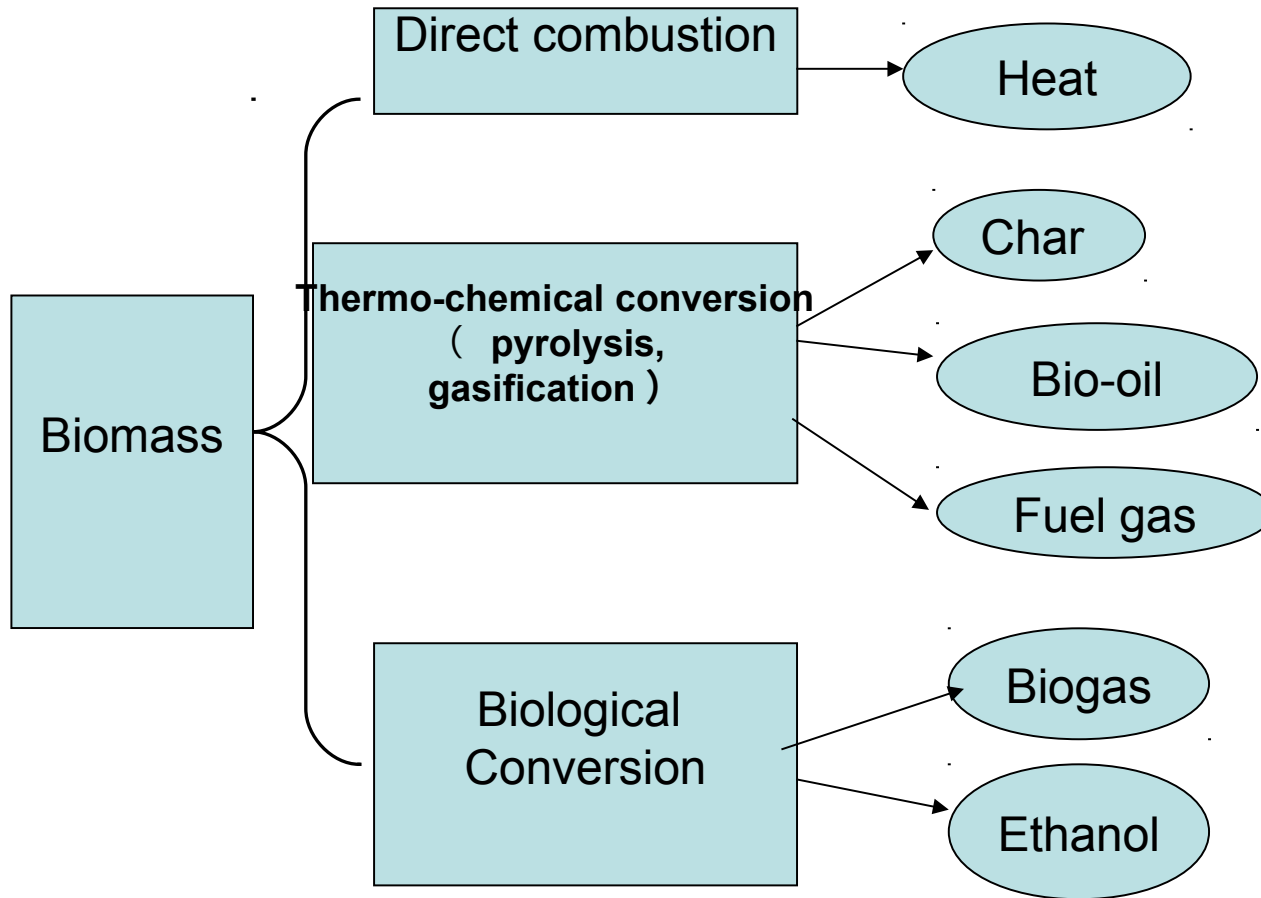
生物质能工程研究中心

Biomass Energy Engineering Research Centre,

School of Agriculture and Biology , Shanghai JiaoTong University has a lot of experiences in the field of biomass energy and environment, including characterization of biomass, biomass pyrolysis, biogas ,biochar, gasification, bioethanol, etc.







## 2. Mechanism of biomass pyrolysis



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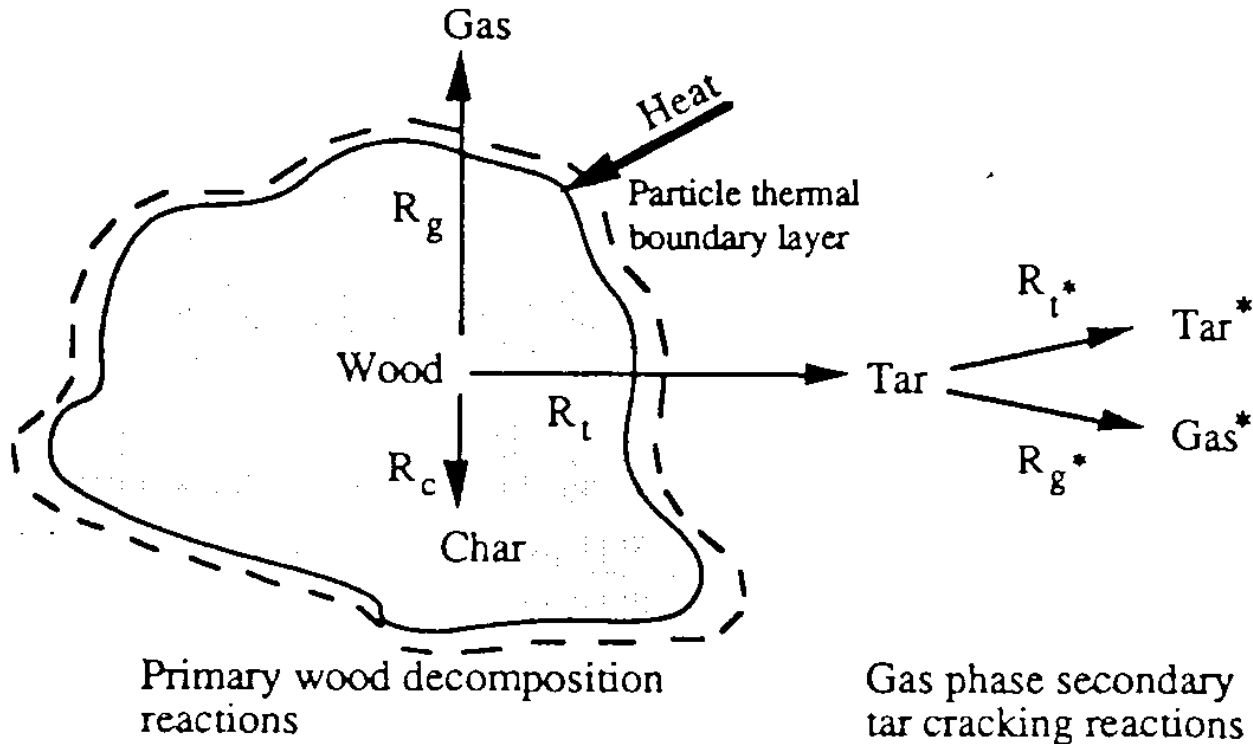


Fig.1 Sketch of a Decomposing Wood Particle  
Including the Reaction Paths Involved

**If the pyrolysis conditions are proper, 100kg biomass can produce 70 kg bio-oil.**



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## 3. Rotating Cone Reactor

- It was key project of Ministry of Science & Technology of China. Professor Ronghou Liu was Vice coordinator.
- The biomass throughput: 50 kg/h
- The bio-oil yield : 53%





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## 4. Fluidized bed reactor for biomass fast pyrolysis for bio-oil production developed by SJTU

Biomass  
throughput: 1-5 kg/  
h;

Reactor  
Temperature: 400-  
600°C

Biomass particle  
size: <2mm







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# \* Effect of hot vapor filtration on the characterization of bio-oil from rice husks with fast pyrolysis in a fluidized-bed reactor



Bioresource Technology 102 (2011) 6178–6185



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Bioresource Technology

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## Effect of hot vapor filtration on the characterization of bio-oil from rice husks with fast pyrolysis in a fluidized-bed reactor

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### Research article

## Effect of temperature of ceramic hot vapor filter in a fluidized bed reactor on chemical composition and structure of bio-oil and reaction mechanism of pine sawdust fast pyrolysis

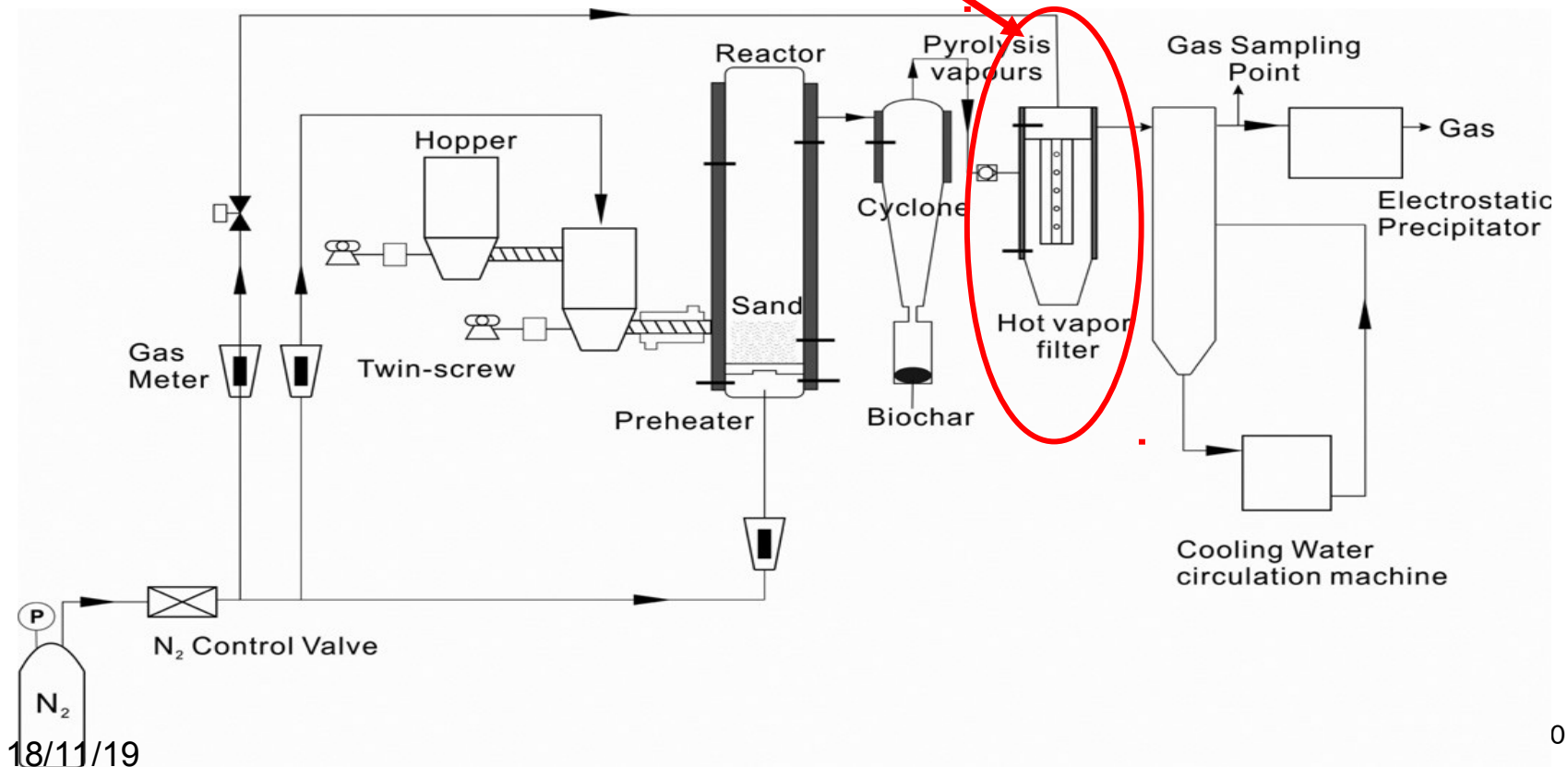
Yuanfei Mei, Ronghou Liu<sup>\*</sup>

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\*Effect of hot vapor filtration on the characterization of bio-oil from rice husks with fast pyrolysis in a fluidized-bed reactor



# Yield and physicochemical properties of bio-oil at condenser

Yield and physicochemical properties of the bio-oil at the condenser and the EP.

	C <sub>1</sub> <sup>c</sup>	C <sub>2</sub> <sup>c</sup>	F <sub>1</sub> <sup>c</sup>	F <sub>2</sub> <sup>c</sup>
Water content(wt.%)	64.41 ± 0.16	10.77 ± 0.10	75.09 ± 0.42	9.19 ± 0.08
Yield of bio-oil (wt.%)	57.3	42.7	60.5	39.5
Ratio of collected water content of oil <sup>a</sup>	88.9	11.1	92.7	7.3
C (wt.%)	17.07	60.95	10.67	66.56
H (wt.%)	10.76	7.26	11.23	7.50
N (wt.%)	<0.3	0.94	<0.3	1.30
O <sup>b</sup> (wt.%)	71.87	30.85	77.80	24.65
pH	2.84	4.10	3.37	4.40
Density (g/cm <sup>3</sup> )	1.0705	1.1550	1.0392	1.1766
High heating value (MJ/kg)	–	22.06	–	23.86
Na content (ppm)	46	38	19	36
K content (ppm)	19	116	13	41
Ca content (ppm)	82	60	57	23
Mg content (ppm)	8	8	8	1

<sup>a</sup> The total water yield during the reaction process is equal to the sum of the product of mass and water content at each condenser. The ratio of the collected water content of oil for each condenser is equal to the collected water yield at each condenser divided by the total water yield.

<sup>b</sup> By difference.

<sup>c</sup> C<sub>1</sub>, C<sub>2</sub> were the bio-oil condensed in the condenser and EP when using the cyclone only to remove the solid particle, and F<sub>1</sub>, F<sub>2</sub> were the bio-oil condensed in the condenser and EP when using the cyclone coupled with HVF.

## Conclusion:


It was found that the total bio-oil yield decreased and that the bio-oil has a higher water content, higher pH value, and lower alkali metal content when a HVF is used in the system.



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# \*Effect of Selective Condensation on the Characterization of Bio-oil from Pine Sawdust Fast Pyrolysis Using a Fluidized-Bed Reactor

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Published on Web 11/11/2010

**energy&fuels**  
article

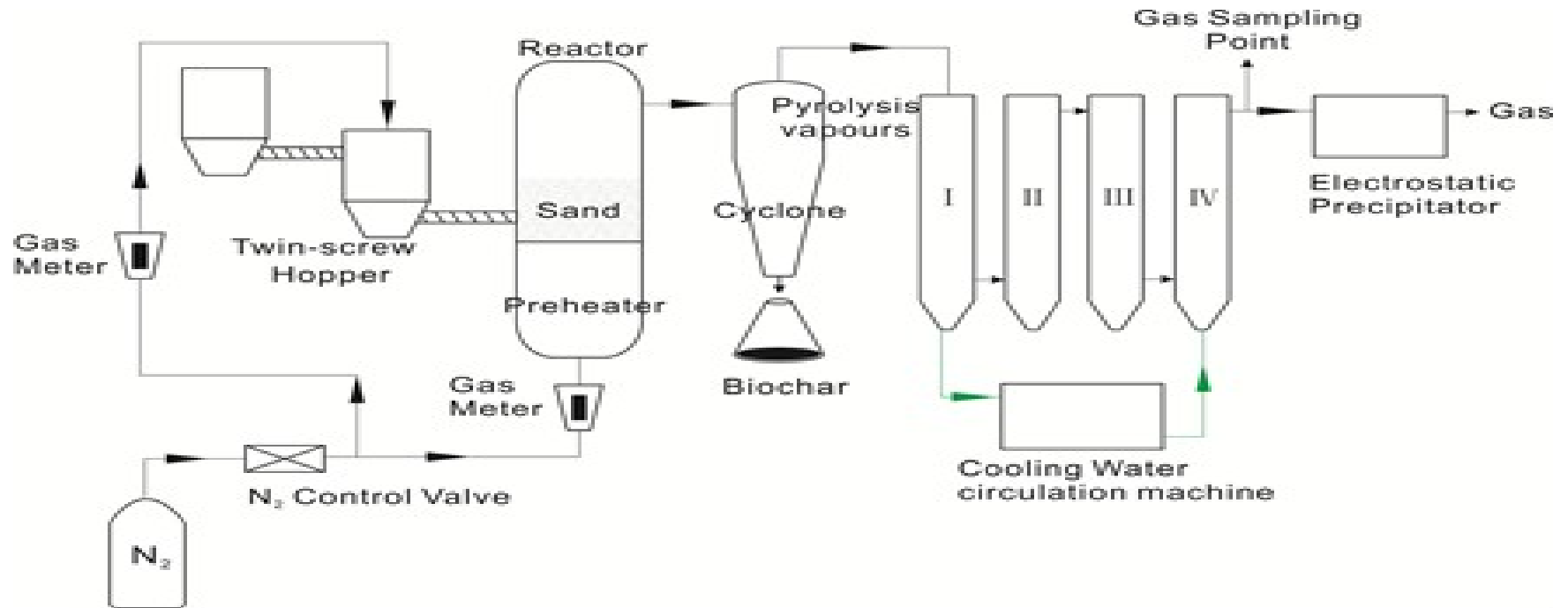
## Effect of Selective Condensation on the Characterization of Bio-oil from Pine Sawdust Fast Pyrolysis Using a Fluidized-Bed Reactor

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*Received September 4, 2010. Revised Manuscript Received October 25, 2010*





**The flow chart of the fluidized bed reactor fast pyrolysis system**



## (1) Yield and the Water Content of the Bio-oil at Different Condensers

Yield and the Water Content of the Bio-oil at Different Condensers

	Condenser 1 <sup>#</sup>	Condenser 2 <sup>#</sup>	Condenser 3 <sup>#</sup>	Condenser 4 <sup>#</sup>	Condenser 5 <sup>#</sup>
Yield of bio-oil (wt/%)	65.3	1.8	1.2	11.3	20.4
Water content(wt/%)	33.21	7.82	7.45	7.35	7.45
Ratio of collected water content of oil <sup>a</sup>	86.2	0.6	0.4	3.3	9.5

Note: <sup>a</sup> The total water yield during the reaction process was equal to the sum of the product of mass and water content at each condenser. The ratio of the collected water content of oil for each condenser is equal to the collected water yield at each condenser divided by the total water yield .

**Conclusion 1** : The total bio-oil, the gases and the char yields were 41.5%, 43.3%, 15.2% respectively ; and 86.2 wt % water steam was condensed in condenser 1.



## (2) Other properties

### pH Value of the Bio-oil

	1 <sup>#</sup>	2 <sup>#</sup>	3 <sup>#</sup>	4 <sup>#</sup>	5 <sup>#</sup>
pH	2.66	2.73	2.78	2.78	2.78

### Higher Heating Value (HHV) of the Bio-oil

	1 <sup>#</sup>	2 <sup>#</sup>	3 <sup>#</sup>	4 <sup>#</sup>	5 <sup>#</sup>
HHV (MJ/Kg)	14.9	22.6	22.9	22.7	23.5

### The Effect of Temperature on the Viscosity of Bio-oil

	20 °C	30 °C	40 °C	50 °C	60 °C	70 °C	80 °C	90 °C
Viscosity of bio-oil 1 <sup>#</sup> (mm <sup>2</sup> /s)	9.10	1.95	1.35	1.21	0.94	0.63	0.54	0.53
Viscosity of bio-oil 4 <sup>#</sup> (mm <sup>2</sup> /s)	938.13	326.09	142.38	69.25	38.01	12.93	7.26	5.80
Viscosity of bio-oil 5 <sup>#</sup> (mm <sup>2</sup> /s)	1210.97	397.44	175.48	82.50	46.87	26.88	17.48	12.62

**Conclusion 2:** The bio-oil condensed in the later condensers has a lower water content, higher pH value, higher heating value, higher kinetic viscosity compared to the first one.



### (3) GC-MS Results

**Table 8. Components of Bio-oil from Pine Sawdust Pyrolysis and Their Relative Mass Contents Detected by GC-MS**

Peak NO.	Main identified compounds	RTA(min)	mol mass	Relative mass content (%)		
				1#	4#	5#
1	Ethynyl isopropyl ketone	3.552	96	0.15		
2	1,3-dione-4-Cyclopentene	3.642	96	1.21	0.21	0.2
3	Cyclopentanone	3.883	84	4.98		
4	2(5H)-Furanone	3.896	84		3.5	2.67
5	2-Methyl-2-cyclopentenone	4.124	96	3.92	1.41	1.24
6	1-(2-furanyl)-Ethanone,	4.227	110	1.18	0.32	0.38
7	3-methyl- 2,4-Pentanedione	4.314	114		0.27	
8	3-methyl- 2,5-Furandione	4.308	112	0.73		0.45
9	2-methyl-Cyclopentanone	4.448	98	9.98	6.68	6.11
10	Bicyclo[3.1.0]hexan-2-one	4.5	96			0.24

**Conclusion 2:** GC-MS showed that 102 types of chemical compounds were detected and most of the compounds were condensed at different condensers. The selective condensation is useful to separate the water and chemical compounds from bio-oil compared with direct contacting condensing.





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BBS 2017 , Shanghai, April 16-17,2017

# 5. Performance of a commercial-scale biomass fast pyrolysis plant for bio-oil production



Full Length Article

## Performance of a commercial-scale biomass fast pyrolysis plant for bio-oil production

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### ARTICLE INFO

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Keywords:  
Fast pyrolysis  
Bio-oil  
Downdraft circulating fluidized bed reactor  
Rice husks

### ABSTRACT

A commercial-scale biomass fast pyrolysis plant, based on downdraft circulating fluidized bed technology with biomass throughput of  $1\text{--}3\text{ t h}^{-1}$ , has been developed for bio-oil production and its performance has been investigated. The technological process consists of six parts: a feeding system, a heat carrier system, a reactor system, a cyclone system, a condensation system and a carbon separating system. The plant has four circulation systems: circulation of a heat carrier, quenching materials (bio-oil), cooling water and non-condensable gas. The bio-oil, raw material (rice husks), char and non-condensable gas samples were analyzed using GC-MS, FTIR, and SEM to characterize the physical properties and chemical composition. Results showed that the operation of the plant was stable. At  $550\text{ }^{\circ}\text{C}$ , the highest yield of bio-oil obtained was  $48.1\text{ wt}\%$  with char, and non-condensable gas yields of  $26.0\text{ wt}\%$  and  $25.9\text{ wt}\%$ , respectively. GC-MS results revealed that the composition of the bio-oil was complicated and the most abundant compound category was phenolics ( $14.92\%$ ). The char had complex pore structure by SEM analysis, which can be collected as a resource for further comprehensive utilization.

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Research article

## Bio-oil production from fast pyrolysis of rice husk in a commercial-scale plant with a downdraft circulating fluidized bed reactor

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Key Laboratory of Urban Agriculture (South), Ministry of Agriculture, 800 Dongchuan Road, Shanghai 200240, PR China

### ARTICLE INFO

Keywords:  
Fast pyrolysis  
Bio-oil  
Downdraft circulating fluidized bed reactor  
Rice husk  
Commercial-scale plant

### ABSTRACT

Bio-oil, a promising candidate to replace fossil fuels, has received considerable attention for its sustainability, resource diversity and environmental benefits. Industrial production of bio-oil is urgently needed. In this study, a downdraft circulating fluidized bed reactor commercial-scale fast pyrolysis plant with biomass throughput of  $1\text{--}3\text{ t h}^{-1}$  is studied. Rice husk was processed at a fast pyrolysis temperature of  $550\text{ }^{\circ}\text{C}$  to evaluate the plant operation status. The system was continuously operated for  $80.42\text{ h}$ . The thermal properties of the feedstock (rice husk), dust (separated from feedstock), char and heat carrier were analyzed and the bio-oil properties such



## 5.1 Financial support

**Project Title :** Development of Equipment for Biomass Fast Pyrolysis for Bio-oil Production and its Demonstration in Thousand Ton Scale

**Project type :** The National Science and Technology Supporting Plan;  
**Ministry of Science and Technology of China**

**Organizer:** Shanghai JiaoTong University

**Partners:** 1) Zhejiang University

2) Shandong University of Technology

3) Guangzhou Institute of Energy Conversion, Chinese Academy of Science

4) University of Science and Technology of China

5) University of Science and Technology of South China

6) Company

**Coordinator of the project:** Ronghou Liu

**Period :** January 2011-December 2013



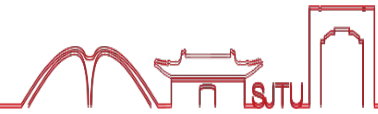
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## 5.2 Pyrolysis plant

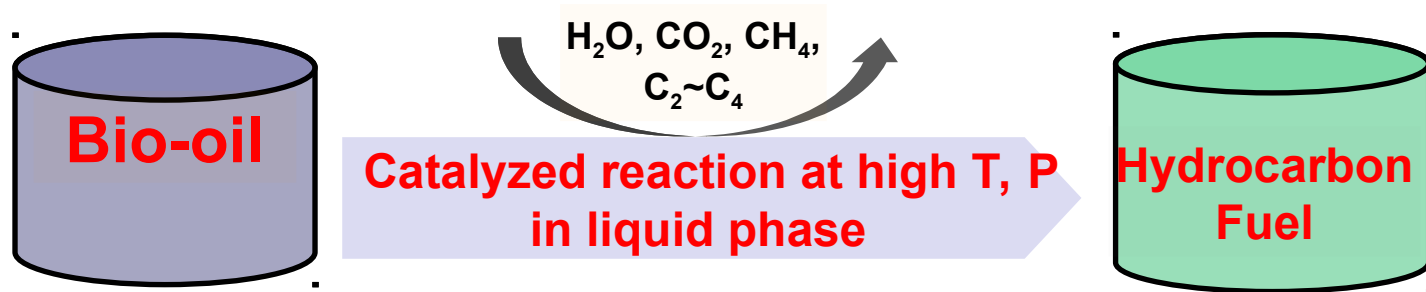
**A commercial-scale biomass fast pyrolysis plant, based on downdraft circulating fluidized bed technology with biomass throughput of 1–3 T /h (Bio-oil yield: 10000 t/a) has been jointly developed and built in Company and Shanghai Jiao Tong University, China for bio-oil production.**





### What is HDO?

--Hydrodeoxygenation



### Why HDO?

- Hydrodeoxygenation is one of the most feasible upgrading method.



## 7.1 Bioethanol

Available online at [www.sciencedirect.com](http://www.sciencedirect.com)



Bioresource Technology 99 (2008) 847–854

BIORESOURCETECHNOLOGY

### Impacts of main factors on bioethanol fermentation from stalk juice of sweet sorghum by immobilized *Saccharomyces cerevisiae* (CICC 1308)

Ronghou Liu \*, Fei Shen

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Received 17 October 2006; received in revised form 17 January 2007; accepted 17 January 2007  
Available online 13 March 2007

#### Abstract

In order to attain a higher ethanol yield and faster ethanol fermentation rate, orthogonal experiments of ethanol fermentation with immobilized yeast from stalk juice of sweet sorghum were carried out in the shaking flasks to investigate the effect of main factors, namely, fermentation temperature, agitation rate, particles stuffing rate and pH on ethanol yield and CO<sub>2</sub> weight loss rate. The range analysis and analysis of variance (ANOVA) were applied for the results of orthogonal experiments. Results showed that the optimal condition for bioethanol fermentation should be A<sub>4</sub>B<sub>3</sub>C<sub>3</sub>D<sub>4</sub>, namely, fermentation temperature, agitation rate, particles stuffing rate and pH were 37 °C, 200 rpm, 25% and 5.0, respectively. The verification experiments were carried out in shaking flasks and 5 L bioreactor at the corresponding parameters. The results of verification experiments in the shaking flasks showed that ethanol yield and CO<sub>2</sub> weight loss rate were 0.877% and 4.1020 g/h, respectively. The results of ethanol fermentation in the 5 L bioreactor showed that ethanol yield and CO<sub>2</sub> weight loss rate were 0.877% and 4.1020 g/h, respectively.

This paper has been Top 20 Articles, in the Domain of Article 17360181, Since its Publication (2008)

#### 1. Introduction

Ethanol production as an alternative fuel energy resource has been a subject of great interest since the oil crisis of the 1970s (Tao et al., 2005). Therefore, a strong need exists for efficient ethanol production with low cost in raw material and production process. The varied raw materials used in the production of ethanol via fermentation are conveniently classified into three main types of raw materials: sugars, starches, and cellulose materials. Sugars (from sugarcane, sugar beets, sweet sorghum, molasses, and fruits) can be converted into ethanol directly. Starches (from corn, cassava, potatoes, and root crops) must firstly be hydrolyzed to fermentable sugars by the action of enzymes from

malt or molds. Cellulose (from wood, agricultural residues, waste sulfite liquor from pulp, and paper mills) must likewise be converted into sugars, generally by the action of mineral acids. Once simple sugars are formed, enzymes from microorganisms can readily ferment them to ethanol (Lin and Tanaka, 2006). As for materials, one of the prime sources being investigated for ethanol is sweet sorghum. Sweet sorghum (*Sorghum bicolor* (L.) Moench) is a high biomass- and sugar-yielding crops (Bryan, 1990), meantime, the stalk of sweet sorghum contains quite a few quantities of soluble (glucose and sucrose) and insoluble carbohydrates (cellulose and hemicellulose) (Jasberg et al., 1983). Therefore, of many crops currently being investigated for energy and industry, sweet sorghum is one of the most promising, particularly for ethanol production (Gnansounou et al., 2005).

The advantages of immobilized cells over free cell systems have been extensively reported (Blancas et al., 2007).

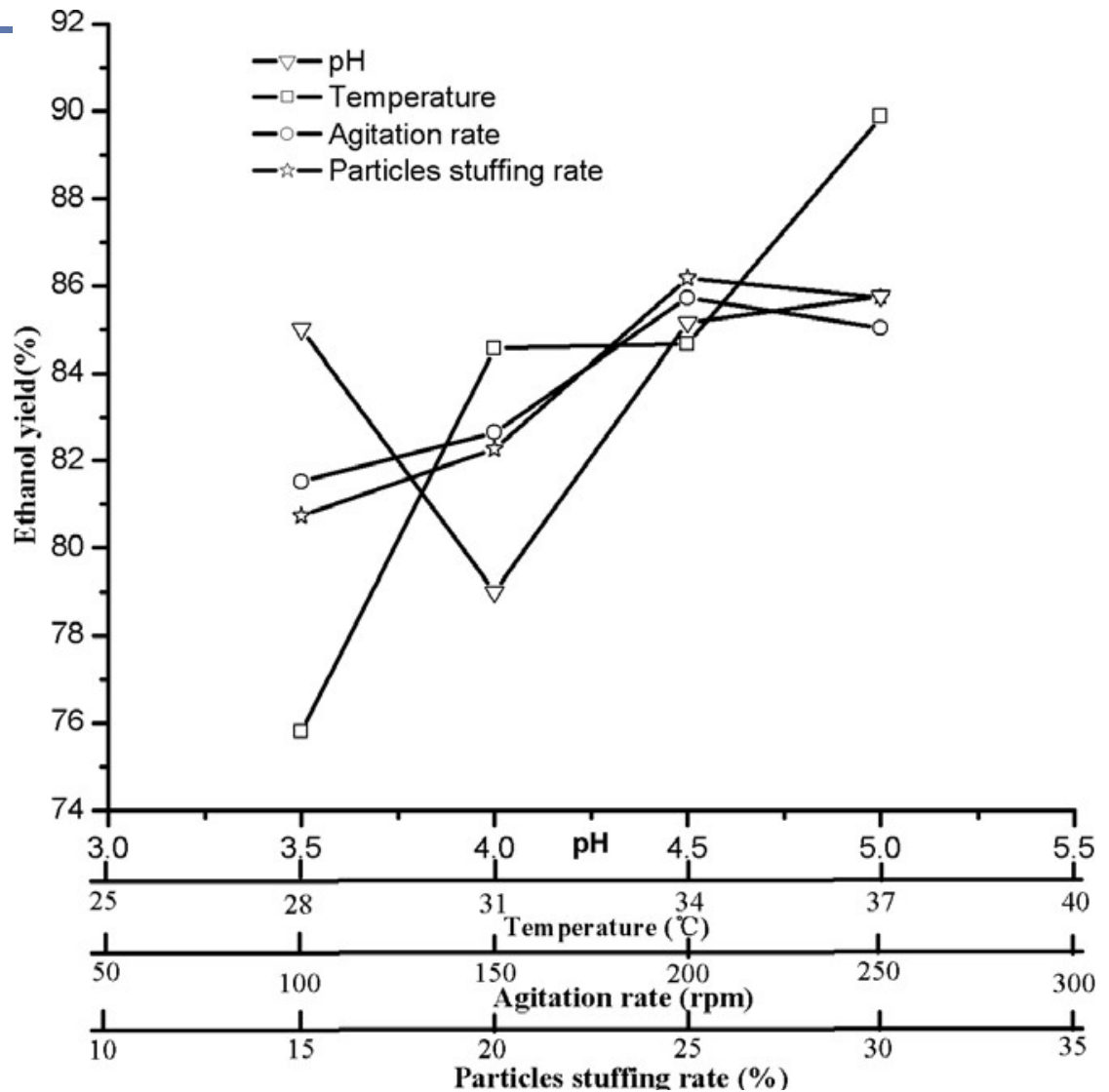
\* Corresponding author. Tel.: +86 21 64783844; fax: +86 21 64193285.



Optimal condition for  
bioethanol  
fermentation:

Fermentation  
temperature: 37 °C ,  
Agitation rate: 200 rpm,

Particles stuffing  
rate: 25%,  
pH 5.0.  
Ethanol yield: 98.07%,  
Fermentation time: 11  
h.





## 7.2.Biogas Technology

# Biogas production from undiluted chicken manure and maize silage: A study of ammonia inhibition in high solids anaerobic digestion

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# Objectives:

- To evaluate the multi-inhibited AD system using CM and MS as the feedstock without any water addition;
- To determine the thresholds for ammonia inhibition/toxicity;

## Conclusions :

- Methanogenesis was totally inhibited at TAN > 9 g N L<sup>-1</sup>. <sup>14</sup>C isotope labelling showed the predominant methanogenic pathway at high TAN was hydrogenotrophic.

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Biogas production from undiluted chicken manure and maize silage: A study of ammonia inhibition in high solids anaerobic digestion



Chen Sun<sup>a,b,c</sup>, Weixing Cao<sup>a,c</sup>, Charles J. Banks<sup>b</sup>, Sonia Heaven<sup>b</sup>, Ronghou Liu<sup>a,b,c,\*</sup>

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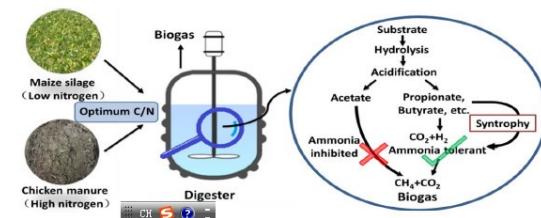
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### HIGHLIGHTS

- Stable co-digestion of up to 20% chicken manure on VS basis with maize silage.
- Threshold and total inhibition of biogas production occurred at 7 and 9 g N L<sup>-1</sup>.
- Dominant hydrogenotrophic methanogenesis reverts to acetoclastic on lower N input.
- Loss of methanogenesis led to total VFA > 60 g L<sup>-1</sup> before buffering failed.
- Sub-optimal solids breakdown as a result of multi-inhibition.

### GRAPHICAL ABSTRACT





# Impacts of Alkaline Hydrogen Peroxide Pretreatment on Chemical Composition and Biochemical Methane Potential of Agricultural Crop Stalks

Chen Sun,<sup>†,‡,§</sup> Ronghou Liu,<sup>\*,†,§</sup> Weixing Cao,<sup>§</sup> Renzhan Yin,<sup>||</sup> Yuanfei Mei,<sup>†,‡,§</sup> and Le Zhang<sup>†,§</sup>

## Objective:

to increase bio-digestibility and methane yield from crop residues via pretreatment

## Results and conclusions:

The AHP pretreatment could:

- break down esterified( 酯化) and etherified ( 醚化) linkage in lignocellulose;
- recover 90% of glucose and 80% of xylose (木糖) ;
- remove 30%-50% of lignin;
- increase methane yield and bio-digestibility for certain biomass.

It is necessary to utilize the liquid waste from the pretreatment.

### Impacts of Alkaline Hydrogen Peroxide Pretreatment on Chemical Composition and Biochemical Methane Potential of Agricultural Crop Stalks

Chen Sun,<sup>†,‡,§</sup> Ronghou Liu,<sup>\*,†,§</sup> Weixing Cao,<sup>§</sup> Renzhan Yin,<sup>||</sup> Yuanfei Mei,<sup>†,‡,§</sup> and Le Zhang<sup>†,§</sup>

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**ABSTRACT:** Lignocellulosic stalks of three kinds of monocotyledonous (wheat, maize, and rice) and two kinds of dicotyledonous crops (legume and ornamental) underwent 30 H<sub>2</sub>O<sub>2</sub> pretreatment at pH 11.0 and 35 °C with 10% (w/v) biomass loading. Chemical composition analysis and biochemical methane potential (BMP) assays were carried out for biomass before and after pretreatment, in order to illustrate the impacts on biomass utilization efficiency caused by the alkaline hydrogen peroxide (AHP) pretreatment. The AHP pretreatment could recover about 90% of glucose and 80% of xylose, and remove about 30%–50% of the lignin in monocotyledonous and dicotyledonous crop stalks, respectively. On the basis of volatile acid (VA) added into the pretreatment system, the chemical BMP and digestible fraction of crop stalks increased from 179.2 ± 12.0 mL CH<sub>4</sub>/g VS to 244.2 ± 6.0 mL CH<sub>4</sub>/g VS and from 36.0 to 48.7%, respectively. For the purpose of full utilization, the theoretical methane potential of liquid waste generated from the AHP pretreatment was investigated. Theoretically, around 90 and 41 mL CH<sub>4</sub>/g VS from liquid waste of monocotyledonous and dicotyledonous crop stalks could be produced, respectively. Besides, chemical composition and structural changes showed that AHP pretreatment could break down esterified and etherified linkage in lignocellulosic matrix.

#### 1. INTRODUCTION

Lignocellulosic materials such as agricultural crop stems and stalks are renewable resources in the world. They mainly consist of cellulose, hemicellulose, and lignin, and are considered as potential sources of biogas.<sup>1</sup> However, the lignocellulosic materials are difficult to be degraded by anaerobic bacteria because of their complex organic polymer structure.<sup>2,3</sup> The close physical and chemical linkages among the cellulose, hemicellulose, and lignin in lignocellulosic materials is a major barrier to their efficient utilization.<sup>4</sup> The major degradation pretreatment of lignocellulosic material is to be one of the hot spots in the area of biogas production in biorefinery technology.<sup>5</sup> There are numerous pretreatment methods for lignocellulosic materials, and they can be classified as physical (explosive, steam, etc.), chemical (acid, alkali, oxidative, etc.), and biological methods.<sup>6</sup> One of the most promising chemical methods for degradation is alkaline hydrogen peroxide (AHP) pretreatment.<sup>7</sup> It was reported that the phenolic acids of lignin had a high tendency to decolor in AHP solution.<sup>8</sup> During AHP pretreatment, the peroxide plays the role of oxidant,<sup>9</sup> which takes part in the current degradation process and has been widely used to bleach highlights wood pulp in the paper-making industry. The role of alkali is to reduce or to remove lignin, acetyl, and other anionic

substitution in hemicellulosic portions of biomass by swelling, solubilization, and degradation, so that the accessibility and digestibility of hemicellulose will be enhanced.<sup>10</sup> It is reported that the AHP pretreatment can remove a significant amount of lignin and glucanase but cause little degradation on cellulose.<sup>11</sup> Guo et al. (2002) have proven that AHP pretreatment is better than alkali pretreatment on the basis of methane yield.<sup>12</sup> This degradation effect caused by AHP treatment is strongly dependent on the pH of the reaction conditions, with an optimum at pH 11.0–11.4<sup>13</sup>, which can also prevent coagulation of hemicellulose.<sup>14</sup> Under this alkaline condition, hydrogen peroxide reacts with both aliphatic and aromatic structures of lignin, leading to depolymerization.<sup>15</sup>

As a promising method, lots of studies have been done on the AHP treatment process conditions in order to improve its efficiency on degradation, sugar recovery, and biogas production. Mass and Lalonde (2011) found that substrate of 2% wheat straw by 20% H<sub>2</sub>O<sub>2</sub> solution at 60 °C with pH 11.0 could reach 77% reduction, 65% sugar, and 90% saccharification degree.<sup>16</sup> Tanskanen et al. (2000) used 1% (v/v) H<sub>2</sub>O<sub>2</sub> and 1 wt % NaOH solution which was actually a mild AHP

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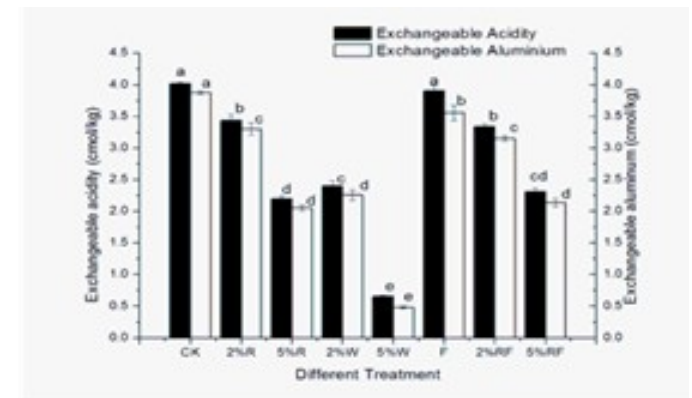
## 7.3. Biochar Application for Soil Amendment and Heavy metal removal

-863 Project by MOST

1) Developed a biochar application machine:

Scale : 4753.8-34185.2 kg/h

2) The effect of biochar on soil and plant growth



Wood sawdust biochar could reduce the exchangeable acidity and aluminum by 84% and 88%, respectively at the 5% biochar amendment level.



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# Thank You!

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